#### 2.4 MUNICIPAL SOLID WASTE LANDFILLS

### 2.4.1 General1-4

A municipal solid waste (MSW) landfill unit is a discrete area of land or an excavation that receives household waste, and that is not a land application unit, surface impoundment, injection well, or waste pile. An MSW landfill unit may also receive other types of wastes, such as commercial solid waste, nonhazardous sludge, and industrial solid waste. The municipal solid waste types potentially accepted by MSW landfills include (most landfills accept only a few of the following categories):

- MSW.
- · Household hazardous waste,
- Municipal sludge,
- Municipal waste combustion ash,
- Infectious waste,
- Waste tires.
- Industrial non-hazardous waste,
- Conditionally exempt small quantity generator (CESQG) hazardous waste,
- Construction and demolition waste,
- Agricultural wastes,
- · Oil and gas wastes, and
- Mining wastes.

In the United States, approximately 57 percent of solid waste is landfilled, 16 percent is incinerated, and 27 percent is recycled or composted. There were an estimated 2,500 active MSW landfills in the United States in 1995. These landfills were estimated to receive 189 million megagrams (Mg) (208 million tons) of waste annually, with 55 to 60 percent reported as household waste, and 35 to 45 percent reported as commercial waste.

## 2.4.2 Process Description<sup>2,5</sup>

There are three major designs for municipal landfills. These are the area, trench, and ramp methods. All of these methods utilize a three step process, which includes spreading the waste, compacting the waste, and covering the waste with soil. The trench and ramp methods are not commonly used, and are not the preferred methods when liners and leachate collection systems are utilized or required by law. The area fill method involves placing waste on the ground surface or landfill liner, spreading it in layers, and compacting with heavy equipment. A daily soil cover is spread over the compacted waste. The trench method entails excavating trenches designed to receive a day's worth of waste. The soil from the excavation is often used for cover material and wind breaks. The ramp method is typically employed on sloping land, where waste is spread and compacted similar to the area method, however, the cover material obtained is generally from the front of the working face of the filling operation.

Modern landfill design often incorporates liners constructed of soil (i.e., recompacted clay), or synthetics (i.e., high density polyethylene), or both to provide an impermeable barrier to leachate (i.e., water that has passed through the landfill) and gas migration from the landfill.

## 2.4.3 Control Technology<sup>1,2,6</sup>

The Resource Conservation and Recovery Act (RCRA) Subtitle D regulations promulgated on October 9, 1991 require that the concentration of methane generated by MSW landfills not exceed 25 percent of the lower explosive limit (LEL) in on-site structures, such as scale houses, or the LEL at the facility property boundary.

The New Source Performance Standards (NSPS) and Emission Guidelines for air emissions from MSW landfills for certain new and existing landfills were published in the Federal Register on March 1, 1996. The regulation requires that Best Demonstrated Technology (BDT) be used to reduce MSW landfill emissions from affected new and existing MSW landfills emitting greater than or equal to 50 Mg/yr (55 tons/yr) of non-methane organic compounds (NMOCs). The MSW landfills that are affected by the NSPS/Emission Guidelines are each new MSW landfill, and each existing MSW landfill that has accepted waste since November 8, 1987, or that has capacity available for future use. The NSPS/Emission Guidelines affect landfills with a design capacity of 2.5 million Mg (2.75 million tons) or more. Control systems require: (1) a well-designed and well-operated gas collection system, and (2) a control device capable of reducing NMOCs in the collected gas by 98 weight-percent.

Landfill gas (LFG) collection systems are either active or passive systems. Active collection systems provide a pressure gradient in order to extract LFG by use of mechanical blowers or compressors. Passive systems allow the natural pressure gradient created by the increase in pressure created by LFG generation within the landfill to mobilize the gas for collection.

LFG control and treatment options include (1) combustion of the LFG, and (2) purification of the LFG. Combustion techniques include techniques that do not recover energy (i.e., flares and thermal incinerators), and techniques that recover energy (i.e., gas turbines and internal combustion engines) and generate electricity from the combustion of the LFG. Boilers can also be employed to recover energy from LFG in the form of steam. Flares involve an open combustion process that requires oxygen for combustion, and can be open or enclosed. Thermal incinerators heat an organic chemical to a high enough temperature in the presence of sufficient oxygen to oxidize the chemical to carbon dioxide (CO<sub>2</sub>) and water. Purification techniques can also be used to process raw landfill gas to pipeline quality natural gas by using adsorption, absorption, and membranes.

#### 2.4.4 Emissions<sup>2,7</sup>

Methane ( $CH_4$ ) and  $CO_2$  are the primary constituents of landfill gas, and are produced by microorganisms within the landfill under anaerobic conditions. Transformations of  $CH_4$  and  $CO_2$  are mediated by microbial populations that are adapted to the cycling of materials in anaerobic environments. Landfill gas generation, including rate and composition, proceeds through four phases. The first phase is aerobic [i.e., with oxygen ( $O_2$ ) available] and the primary gas produced is  $CO_2$ . The second phase is characterized by  $O_2$  depletion, resulting in an anaerobic environment, where large amounts of  $CO_2$  and some hydrogen ( $H_2$ ) are produced. In the third phase,  $CH_4$  production begins, with an accompanying reduction in the amount of  $CO_2$  produced. Nitrogen ( $N_2$ ) content is initially high in landfill gas in the first phase, and declines sharply as the landfill proceeds through the second and third phases. In the fourth phase, gas production of  $CH_4$ ,  $CO_2$ , and  $N_2$  becomes fairly steady. The total time and phase duration of gas generation varies with landfill conditions (i.e., waste composition, design management, and anaerobic state).

Typically, LFG also contains a small amount of non-methane organic compounds (NMOC). This NMOC fraction often contains various organic hazardous air pollutants (HAP), greenhouse gases (GHG), and compounds associated with stratospheric ozone depletion. The NMOC fraction also contains volatile organic compounds (VOC). The weight fraction of VOC can be determined by subtracting the weight fractions of individual compounds that are non-photochemically reactive (i.e., negligibly-reactive organic compounds as defined in 40 CFR 51.100).

Other emissions associated with MSW landfills include combustion products from LFG control and utilization equipment (i.e., flares, engines, turbines, and boilers). These include carbon monoxide (CO), oxides of nitrogen ( $NO_x$ ), sulfur dioxide ( $SO_2$ ), hydrogen chloride (HCl), particulate matter (PM) and other combustion products (including HAPs). PM emissions can also be generated in the form of fugitive dust created by mobile sources (i.e., garbage trucks) traveling along paved and unpaved surfaces. The reader should consult AP-42 Volume I Sections 13.2.1 and 13.2.2 for information on estimating fugitive dust emissions from paved and unpaved roads.

The rate of emissions from a landfill is governed by gas production and transport mechanisms. Production mechanisms involve the production of the emission constituent in its vapor phase through vaporization, biological decomposition, or chemical reaction. Transport mechanisms involve the transportation of a volatile constituent in its vapor phase to the surface of the landfill, through the air boundary layer above the landfill, and into the atmosphere. The three major transport mechanisms that enable transport of a volatile constituent in its vapor phase are diffusion, convection, and displacement.

2.4.4.1 Uncontrolled Emissions — To estimate uncontrolled emissions of the various compounds present in landfill gas, total landfill gas emissions must first be estimated. Uncontrolled CH<sub>4</sub> emissions may be estimated for individual landfills by using a theoretical first-order kinetic model of methane production developed by the EPA.<sup>8</sup> This model is known as the Landfill Air Emissions Estimation model, and can be accessed from the Office of Air Quality Planning and Standards Technology Transfer Network Website (OAQPS TTN Web) in the Clearinghouse for Inventories and Emission Factors (CHIEF) technical area (URL http://www.epa.gov/ttn/chief). The Landfill Air Emissions Estimation model equation is as follows:

$$Q_{CH_4} = L_o R (e^{-kc} - e^{-kt})$$
 (1)

where:

 $Q_{CH_4}$  = Methane generation rate at time t, m<sup>3</sup>/yr;

 $L_0^{\tau}$  = Methane generation potential, m<sup>3</sup> CH<sub>4</sub>/Mg refuse;

R = Average annual refuse acceptance rate during active life, Mg/yr;

e = Base log, unitless;

k = Methane generation rate constant, yr<sup>-1</sup>;

c = Time since landfill closure, yrs (c = 0 for active landfills); and

t = Time since the initial refuse placement, yrs.

It should be noted that the model above was designed to estimate LFG generation and not LFG emissions to the atmosphere. Other fates may exist for the gas generated in a landfill, including capture and subsequent microbial degradation within the landfill's surface layer. Currently, there are no data that adequately address this fate. It is generally accepted that the bulk of the gas generated will be emitted through cracks or other openings in the landfill surface.

Site-specific landfill information is generally available for variables R, c, and t. When refuse acceptance rate information is scant or unknown, R can be determined by dividing the refuse in place by the age of the landfill. If a facility has documentation that a certain segment (cell) of a landfill received *only* nondegradable refuse, then the waste from this segment of the landfill can be excluded from the calculation of R. Nondegradable refuse includes concrete, brick, stone, glass, plaster, wallboard, piping, plastics, and metal objects. The average annual acceptance rate should only be estimated by this method when there is inadequate information available on the actual average acceptance rate. The time variable, t, includes the total number of years that the refuse has been in place (including the number of years that the landfill has accepted waste and, if applicable, has been closed).

Values for variables  $L_o$  and k must be estimated. Estimation of the potential  $CH_4$  generation capacity of refuse ( $L_o$ ) is generally treated as a function of the moisture and organic content of the refuse. Estimation of the  $CH_4$  generation constant (k) is a function of a variety of factors, including moisture, pH, temperature, and other environmental factors, and landfill operating conditions. Specific  $CH_4$  generation constants can be computed by the use of EPA Method 2E (40 CFR Part 60 Appendix A).

The Landfill Air Emission Estimation model includes both regulatory default values and recommended AP-42 default values for  $L_o$  and k. The regulatory defaults were developed for compliance purposes (NSPS/Emission Guideline). As a result, the model contains conservative  $L_o$  and k default values in order to protect human health, to encompass a wide range of landfills, and to encourage the use of site-specific data. Therefore, different  $L_o$  and k values may be appropriate in estimating landfill emissions for particular landfills and for use in an emissions inventory.

Recommended AP-42 defaults include a k value of 0.04/yr for areas recieving 25 inches or more of rain per year. A default k of 0.02/yr should be used in drier areas (<25 inches/yr). An  $L_o$  value of  $100 \text{ m}^3/\text{Mg}$  (3,530 ft $^3/\text{ton}$ ) refuse is appropriate for most landfills. Although the recommended default k and  $L_o$  are based upon the best fit to 21 different landfills, the predicted methane emissions ranged from 38 to 492% of actual, and had a relative standard deviation of 0.85. It should be emphasized that in order to comply with the NSPS/Emission Guideline, the regulatory defaults for k and  $L_o$  must be applied as specified in the final rule.

When gas generation reaches steady state conditions, LFG consists of approximately 40 percent by volume  $CO_2$ , 55 percent  $CH_4$ , 5 percent  $N_2$  (and other gases), and trace amounts of NMOCs. Therefore, the estimate derived for  $CH_4$  generation using the Landfill Air Emissions Estimation model can also be used to represent  $CO_2$  generation. Addition of the  $CH_4$  and  $CO_2$  emissions will yield an estimate of total landfill gas emissions. If site-specific information is available to suggest that the  $CH_4$  content of landfill gas is not 55 percent, then the site-specific information should be used, and the  $CO_2$  emission estimate should be adjusted accordingly.

Most of the NMOC emissions result from the volatilization of organic compounds contained in the landfilled waste. Small amounts may be created by biological processes and chemical reactions within the landfill. The current version of the Landfill Air Emissions Estimation model contains a proposed regulatory default value for total NMOC of 4,000 ppmv, expressed as hexane. However, available data show that there is a range of over 4,400 ppmv for total NMOC values from landfills. The proposed regulatory default value for NMOC concentration was developed for regulatory compliance purposes and to provide the most cost-effective default values on a national basis. For emissions inventory purposes, site-specific information should be taken into account when determining the total NMOC concentration. In the absence of site-specific information, a value of 2,420 ppmv as hexane is suggested for landfills known to have co-disposal of MSW and non-residential waste. If the landfill is known to contain only MSW or

have very little organic commercial/industrial wastes, then a total NMOC value of 595 ppmv as hexane should be used. In addition, as with the landfill model defaults, the regulatory default value for NMOC content must be used in order to comply with the NSPS/Emission Guideline.

If a site-specific total pollutant concentration is available (i.e., as measured by EPA Reference Method 25C), it must be corrected for air infiltration which can occur by two different mechanisms: LFG sample dilution, and air intrusion into the landfill. These corrections require site-specific data for the LFG  $CH_4$ ,  $CO_2$ , nitrogen  $(N_2)$ , and oxygen  $(O_2)$  content. If the ratio of  $N_2$  to  $O_2$  is less than or equal to 4.0 (as found in ambient air), then the total pollutant concentration is adjusted for sample dilution by assuming that  $CO_2$  and  $CH_4$  are the primary (100 percent) constituents of landfill gas, and the following equation is used:

$$C_p$$
 (ppmv) (corrected for air infiltration) = 
$$\frac{C_p \text{ (ppmv) (1 x 10^6)}}{C_{CO_2} \text{ (ppmv) + } C_{CH_4} \text{ (ppmv)}}$$
 (2)

where:

Cp = Concentration of pollutant P in landfill gas (i.e., NMOC as hexane), ppmv;

 $C_{CO_2}$  =  $CO_2$  concentration in landfill gas, ppmv;

 $C_{CH_4}$  =  $CH_4$  Concentration in landfill gas, ppmv; and

 $1 \times 10^6$  = Constant used to correct concentration of P to units of ppmv.

If the ratio of  $N_2$  to  $O_2$  concentrations (i.e.,  $C_{N_2}$ ,  $C_{O_2}$ ) is greater than 4.0, then the total pollutant concentration should be adjusted for air intrusion into the landfill by using equation 2 and adding the concentration of  $N_2$  (i.e.,  $C_{N_2}$ ) to the denominator. Values for  $C_{CO_2}$ ,  $C_{CH_4}$ ,  $C_{N_2}$ ,  $C_{O_2}$ , can usually be found in the source test report for the particular landfill along with the total pollutant concentration data.

To estimate emissions of NMOC or other landfill gas constituents, the following equation should be used:

$$Q_{P} = 1.82 \ Q_{CH_4} * \frac{C_{P}}{(1 \ x \ 10^6)}$$
 (3)

where:

 $Q_P$  = Emission rate of pollutant P (i.e. NMOC),  $m^3/yr$ ;

 $Q_{CH_{\star}} = CH_4$  generation rate, m<sup>3</sup>/yr (from the Landfill Air Emissions Estimation model);

C<sub>P</sub> = Concentration of P in landfill gas, ppmv; and

1.82 = Multiplication factor (assumes that approximately 55 percent of landfill gas is

 $CH_4$  and 45 percent is  $CO_2$ ,  $N_2$ , and other constituents).

Uncontrolled mass emissions per year of total NMOC (as hexane), CO<sub>2</sub>, CH<sub>4</sub>, and speciated organic and inorganic compounds can be estimated by the following equation:

$$UM_{P} = Q_{P} * \left[ \frac{MW_{P} * 1 \text{ atm}}{(8.205 \times 10^{-5} \text{ m}^{3} - \text{atm/gmol} - \text{`K})(1000 \text{g/kg})(273 + \text{T} \text{`K})} \right]$$
(4)

where:

 $UM_{\mathbf{P}} =$ Uncontrolled mass emissions of pollutant P (i.e., NMOC), kg/yr;  $\begin{array}{rcl} UM_P & = \\ MW_P & = \\ Q_P & = \end{array}$ Molecular weight of P, g/gmol (i.e., 86.18 for NMOC as hexane);

NMOC emission rate of P, m<sup>3</sup>/yr; and Temperature of landfill gas, °C.

This equation assumes that the operating pressure of the system is approximately 1 atmosphere. If the temperature of the landfill gas is not known, a temperature of 25°C (77°F) is recommended.

Uncontrolled default concentrations of speciated organics along with some inorganic compounds are presented in Table 2.4-1. These default concentrations have already been corrected for air infiltration and can be used as input parameters to equation 3 or the Landfill Air Emission Estimation model for estimating speciated emissions from landfills when site-specific data are not available. An analysis of the data, based on the co-disposal history (with non-residential wastes) of the individual landfills from which the concentration data were derived, indicates that for benzene, NMOC, and toluene, there is a difference in the uncontrolled concentrations. Table 2.4-2 presents the corrected concentrations for benzene, NMOC, and toluene to use based on the site's co-disposal history.

It is important to note that the compounds listed in Tables 2.4-1 and 2.4-2 are not the only compounds likely to be present in LFG. The listed compounds are those that were identified through a review of the available literature. The reader should be aware that additional compounds are likely present, such as those associated with consumer or industrial products. Given this information, extreme caution should be exercised in the use of the default VOC weight fractions and concentrations given at the bottom of Table 2.4-2. These default VOC values are heavily influenced by the ethane content of the LFG. Available data have shown that there is a range of over 1,500 ppmy in LFG ethane content among landfills.

2.4.4.2 Controlled Emissions — Emissions from landfills are typically controlled by installing a gas collection system, and combusting the collected gas through the use of internal combustion engines, flares, or turbines. Gas collection systems are not 100 percent efficient in collecting landfill gas, so emissions of CH<sub>4</sub> and NMOC at a landfill with a gas recovery system still occur. To estimate controlled emissions of CH<sub>4</sub>, NMOC, and other constituents in landfill gas, the collection efficiency of the system must first be estimated. Reported collection efficiencies typically range from 60 to 85 percent, with an average of 75 percent most commonly assumed. Higher collection efficiencies may be achieved at some sites (i.e., those engineered to control gas emissions). If site-specific collection efficiencies are available (i.e., through a comprehensive surface sampling program), then they should be used instead of the 75 percent average.

Controlled emission estimates also need to take into account the control efficiency of the control device. Control efficiencies based on test data for the combustion of CH<sub>4</sub>, NMOC, and some speciated organics with differing control devices are presented in Table 2.4-3. Emissions from the control devices need to be added to the uncollected emissions to estimate total controlled emissions.

Controlled CH<sub>4</sub>, NMOC, and speciated emissions can be calculated with equation 5. It is assumed that the landfill gas collection and control system operates 100 percent of the time. Minor durations of system downtime associated with routine maintenance and repair (i.e., 5 to 7 percent) will not appreciably effect emission estimates. The first term in equation 5 accounts for emissions from uncollected landfill gas, while the second term accounts for emissions of the pollutant that were collected but not combusted in the control or utilization device:

$$CM_{P} = \left[ UM_{P} * \left( 1 - \frac{\eta_{col}}{100} \right) \right] + \left[ UM_{P} * \frac{\eta_{col}}{100} * \left( 1 - \frac{\eta_{cnt}}{100} \right) \right]$$
 (5)

where:

CMp = Controlled mass emissions of pollutant P, kg/yr;

UMp = Uncontrolled mass emissions of P, kg/yr (from equation 4 or the Landfill Air

Emissions Estimation Model);

 $\eta_{col} =$  Collection efficiency of the landfill gas collection system, percent; and  $\eta_{cnt} =$  Control efficiency of the landfill gas control or utilization device, percent.

Emission factors for the secondary compounds, CO and  $NO_x$ , exiting the control device are presented in Tables 2.4-4 and 2.4-5. These emission factors should be used when equipment vendor guarantees are not available.

Controlled emissions of  $CO_2$  and sulfur dioxide ( $SO_2$ ) are best estimated using site-specific landfill gas constituent concentrations and mass balance methods.<sup>68</sup> If site-specific data are not available, the data in tables 2.4-1 through 2.4-3 can be used with the mass balance methods that follow.

Controlled  $CO_2$  emissions include emissions from the  $CO_2$  component of landfill gas (equivalent to uncontrolled emissions) and additional  $CO_2$  formed during the combustion of landfill gas. The bulk of the  $CO_2$  formed during landfill gas combustion comes from the combustion of the  $CH_4$  fraction. Small quantities will be formed during the combustion of the NMOC fraction, however, this typically amounts to less than 1 percent of total  $CO_2$  emissions by weight. Also, the formation of CO through incomplete combustion of landfill gas will result in small quantities of  $CO_2$  not being formed. This contribution to the overall mass balance picture is also very small and does not have a significant impact on overall  $CO_2$  emissions.

The following equation which assumes a 100 percent combustion efficiency for CH<sub>4</sub> can be used to estimate CO<sub>2</sub> emissions from controlled landfills:

$$CM_{CO_2} = UM_{CO_2} + \left[ UM_{CH_4} * \frac{\eta_{col}}{100} * 2.75 \right]$$
 (6)

where:

 $CM_{CO_2}$  = Controlled mass emissions of  $CO_2$ , kg/yr;

 $UM_{CO_2}$  = Uncontrolled mass emissions of  $CO_2$ , kg/yr (from equation 4 or the Landfill Air

Emission Estimation Model);

 $UM_{CH_4}$  = Uncontrolled mass emissions of  $CH_4$ , kg/yr (from equation 4 on the Landfill Air

Emission Estimation Model);

 $\eta_{col}$  = Efficiency of the landfill gas collection system, percent; and

2.75 = Ratio of the molecular weight of  $CO_2$  to the molecular weight of  $CH_4$ .

To prepare estimates of  $SO_2$  emissions, data on the concentration of reduced sulfur compounds within the landfill gas are needed. The best way to prepare this estimate is with site-specific information on the total reduced sulfur content of the landfill gas. Often these data are expressed in ppmv as sulfur (S). Equations 3 and 4 should be used first to determine the uncontrolled mass emission rate of reduced sulfur compounds as sulfur. Then, the following equation can be used to estimate  $SO_2$  emissions:

$$CM_{SO_2} = UM_S * \frac{\eta_{col}}{100} * 2.0$$
 (7)

where:

 $CM_{SO_2}$  = Controlled mass emissions of  $SO_2$ , kg/yr;

 $UM_S^2$  = Uncontrolled mass emissions of reduced sulfur compounds as sulfur, kg/yr (from

equations 3 and 4);

 $\eta_{col}$  = Efficiency of the landfill gas collection system, percent; and

2.0 = Ratio of the molecular weight of  $SO_2$  to the molecular weight of S.

The next best method to estimate  $SO_2$  concentrations, if site-specific data for total reduced sulfur compounds as sulfur are not available, is to use site-specific data for speciated reduced sulfur compound concentrations. These data can be converted to ppmv as S with equation 8. After the total reduced sulfur as S has been obtained from equation 8, then equations 3, 4, and 7 can be used to derive  $SO_2$  emissions.

$$C_{S} = \sum_{i=1}^{n} C_{P} * S_{P}$$

$$(8)$$

where:

C<sub>S</sub> = Concentration of total reduced sulfur compounds, ppmv as S (for use in equation 3):

Cp = Concentration of each reduced sulfur compound, ppmv;

Sp = Number of moles of S produced from the combustion of each reduced sulfur

compound (i.e., 1 for sulfides, 2 for disulfides); and

n = Number of reduced sulfur compounds available for summation.

If no site-specific data are available, a value of 46.9 ppmv can be assumed for  $C_s$  (for use in equation 3). This value was obtained by using the default concentrations presented in Table 2.4-1 for reduced sulfur compounds and equation 8.

Hydrochloric acid [Hydrogen Chloride (HCl)] emissions are formed when chlorinated compounds in LFG are combusted in control equipment. The best methods to estimate emissions are mass balance methods that are analogous to those presented above for estimating SO<sub>2</sub> emissions. Hence, the best source of data to estimate HCl emissions is site-specific LFG data on total chloride [expressed in ppmv as the chloride ion (Cl<sup>-</sup>)]. If these data are not available, then total chloride can be estimated from data on individual chlorinated species using equation 9 below. However, emission estimates may be

underestimated, since not every chlorinated compound in the LFG will be represented in the laboratory report (i.e., only those that the analytical method specifies).

$$C_{Cl} = \sum_{i=1}^{n} C_{P} * Cl_{P}$$

$$(9)$$

where:

C<sub>Cl</sub> = Concentration of total chloride, ppmv as Cl<sup>-</sup> (for use in equation 3);

Cp = Concentration of each chlorinated compound, ppmv;

Clp = Number of moles of Cl<sup>-</sup> produced from the combustion of each chlorinated

compound (i.e., 3 for 1,1,1-trichloroethane); and

n = Number of chlorinated compounds available for summation.

After the total chloride concentration ( $C_{Cl}$ ) has been estimated, equations 3 and 4 should be used to determine the total uncontrolled mass emission rate of chlorinated compounds as chloride ion ( $UM_{Cl}$ ). This value is then used in equation 10 below to derive HCl emission estimates:

$$CM_{HCl} = UM_{Cl} * \frac{\eta_{col}}{100} * 1.03 * \left(1 - \frac{\eta_{cnt}}{100}\right)$$
 (10)

where:

CM<sub>HCl</sub> = Controlled mass emissions of HCl, kg/yr;

 $UM_{Cl}$  = Uncontrolled mass emissions of chlorinated compounds as chloride, kg/yr (from

equations 3 and 4);

 $\eta_{col}$  = Efficiency of the landfill gas collection system, percent;

 $\eta_{cnt}$  = Ratio of the molecular weight of HCl to the molecular weight of Cl; and Control efficiency of the landfill gas control or utilization device, percent.

In estimating HCl emissions, it is assumed that all of the chloride ion from the combustion of chlorinated LFG constituents is converted to HCl. If an estimate of the control efficiency,  $\eta_{cnt}$ , is not available, then the high end of the control efficiency range for the equipment listed in Table 9 should be used. This assumption is recommended to assume that HCl emissions are not under-estimated.

If site-specific data on total chloride or speciated chlorinated compounds are not available, then a default value of 42.0 ppmv can be used for  $C_{\text{Cl}}$ . This value was derived from the default LFG constituent concentrations presented in Table 2.4-1. As mentioned above, use of this default may produce underestimates of HCl emissions since it is based only on those compounds for which analyses have been performed. The constituents listed in Table 2.4-1are likely not all of the chlorinated compounds present in LFG.

The reader is referred to Sections 11.2-1 (Unpaved Roads, SCC 50100401), and 11-2.4 (Heavy Construction Operations) of Volume I, and Section II-7 (Construction Equipment) of Volume II, of the AP-42 document for determination of associated fugitive dust and exhaust emissions from these emission sources at MSW landfills.

# 2.4.5 Updates Since the Fifth Edition

The Fifth Edition was released in January 1995. This is revision includes major revisions of the text and recommended emission factors conained in the section. The most significant revisions to this section since publication in the Fifth Edition are summarized below.

- The equations to calculate the CH4, CO2 and other constituents were simplified.
- The default L0 and k were revised based upon an expanded base of gas generation data.
- The default ratio of CO2 to CH4 was revised based upon averages observed in available source test reports.
- The default concentrations of LFG constituents were revised based upon additional data.
- Additional control efficiencies were included and existing efficiencies were revised based upon additional emission test data.
- Revised and expanded the recommended emission factors for secondary compounds emitted from typical control devices.

Table 2.4-1. DEFAULT CONCENTRATIONS FOR LFG CONSTITUENTS<sup>a</sup>

(SCC 50100402, 50300603)

(SCC 30)	100402, 50300603)	D.C. 1	
		Default Concentration	Emission Factor
Compound	Molecular Weight	(ppmv)	Rating
1,1,1-Trichloroethane (methyl chloroform) <sup>a</sup>	133.42	0.48	В
1,1,2,2-Tetrachloroethane <sup>a</sup>	167.85	1.11	С
1,1-Dichloroethane (ethylidene dichloride) <sup>a</sup>	98.95	2.35	В
1,1-Dichloroethene (vinylidene chloride) <sup>a</sup>	96.94	0.20	В
1,2-Dichloroethane (ethylene dichloride) <sup>a</sup>	98.96	0.41	В
1,2-Dichloropropane (propylene dichloride) <sup>a</sup>	112.98	0.18	D
2-Propanol (isopropyl alcohol)	60.11	50.1	Е
Acetone	58.08	7.01	В
Acrylonitrile <sup>a</sup>	53.06	6.33	D
Bromodichloromethane	163.83	3.13	C
Butane	58.12	5.03	C
Carbon disulfide <sup>a</sup>	76.13	0.58	C
Carbon monoxide <sup>b</sup>	28.01	141	E
Carbon tetrachloride <sup>a</sup>	153.84	0.004	В
Carbonyl sulfide <sup>a</sup>	60.07	0.49	D
Chlorobenzene <sup>a</sup>	112.56	0.25	C
Chlorodifluoromethane	86.47	1.30	C
Chloroethane (ethyl chloride) <sup>a</sup>	64.52	1.25	В
Chloroform <sup>a</sup>	119.39	0.03	В
Chloromethane	50.49	1.21	В
Dichlorobenzene <sup>c</sup>	147	0.21	Е
Dichlorodifluoromethane	120.91	15.7	A
Dichlorofluoromethane	102.92	2.62	D
Dichloromethane (methylene chloride) <sup>a</sup>	84.94	14.3	A
Dimethyl sulfide (methyl sulfide)	62.13	7.82	С
Ethane	30.07	889	С
Ethanol	46.08	27.2	Е
Ethyl mercaptan (ethanethiol)	62.13	2.28	D
Ethylbenzene <sup>a</sup>	106.16	4.61	В
Ethylene dibromide	187.88	0.001	Е
Fluorotrichloromethane	137.38	0.76	В
Hexane <sup>a</sup>	86.18	6.57	В
Hydrogen sulfide	34.08	35.5	В
Mercury (total) <sup>a,d</sup>	200.61	2.92x10 <sup>-4</sup>	Е

Table 2.4-1. (Concluded)

Compound	Molecular Weight	Default Concentration (ppmv)	Emission Factor Rating
Methyl ethyl ketone <sup>a</sup>	72.11	7.09	A
Methyl isobutyl ketone <sup>a</sup>	100.16	1.87	В
Methyl mercaptan	48.11	2.49	С
Pentane	72.15	3.29	C
Perchloroethylene (tetrachloroethylene) <sup>a</sup>	165.83	3.73	В
Propane	44.09	11.1	В
t-1,2-dichloroethene	96.94	2.84	В
Trichloroethylene (trichloroethene) <sup>a</sup>	131.38	2.82	В
Vinyl chloride <sup>a</sup>	62.50	7.34	В
Xylenes <sup>a</sup>	106.16	12.1	В

NOTE: This is not an all-inclusive list of potential LFG constituents, only those for which test data were available at multiple sites. References 10-67. Source Classification Codes in parentheses.

<sup>&</sup>lt;sup>a</sup> Hazardous Air Pollutants listed in Title III of the 1990 Clean Air Act Amendments.

<sup>&</sup>lt;sup>b</sup> Carbon monoxide is not a typical constituent of LFG, but does exist in instances involving landfill (underground) combustion. Therefore, this default value should be used with caution. Of 18 sites where CO was measured, only 2 showed detectable levels of CO.

 $<sup>^{\</sup>rm c}$  Source tests did not indicate whether this compound was the para- or ortho- isomer. The para isomer is a Title III-listed HAP.

<sup>&</sup>lt;sup>d</sup> No data were available to speciate total Hg into the elemental and organic forms.

Table 2.4-2. DEFAULT CONCENTRATIONS OF BENZENE, NMOC, AND TOLUENE BASED ON WASTE DISPOSAL HISTORY  $^{\rm a}$ 

(SCC 50100402, 50300603)

Pollutant	Molecular Weight	Default Concentration (ppmv)	Emission Factor Rating
Benzene <sup>b</sup>	78.11		
Co-disposal		11.1	D
No or Unknown co-disposal		1.91	В
NMOC (as hexane) <sup>c</sup>	86.18		
Co-disposal		2420	D
No or Unknown co-disposal		595	В
Toluene <sup>b</sup>	92.13		
Co-disposal		165	D
No or Unknown co-disposal		39.3	A

<sup>&</sup>lt;sup>a</sup> References 10-54. Source Classification Codes in parentheses.

<sup>&</sup>lt;sup>b</sup> Hazardous Air Pollutants listed in Title III of the 1990 Clean Air Act Amendments.

<sup>&</sup>lt;sup>c</sup> For NSPS/Emission Guideline compliance purposes, the default concentration for NMOC as specified in the final rule must be used. For purposes not associated with NSPS/Emission Guideline compliance, the default VOC content at co-disposal sites = 85 percent by weight (2,060 ppmv as hexane); at No or Unknown sites = 39 percent by weight 235 ppmv as hexane).

Table 2.4-3. CONTROL EFFICIENCIES FOR LFG CONSTITUENTS<sup>a</sup>

		Control Efficiency (%)		
Control Device	Constituent <sup>b</sup>	Typical	Range	Rating
Boiler/Steam Turbine	NMOC	98.0	96-99+	D
(50100423)	Halogenated Species	99.6	87-99+	D
	Non-Halogenated Species	99.8	67-99+	D
Flare <sup>c</sup>	NMOC	99.2	90-99+	В
(50100410) (50300601)	Halogenated Species	98.0	91-99+	C
	Non-Halogenated Species	99.7	38-99+	С
Gas Turbine	NMOC	94.4	90-99+	E
(50100420)	Halogenated Species	99.7	98-99+	Е
	Non-Halogenated Species	98.2	97-99+	Е
IC Engine (50100421)	NMOC	97.2	94-99+	E
(30100721)	Halogenated Species	93.0	90-99+	E
	Non-Halogenated Species	86.1	25-99+	E

<sup>&</sup>lt;sup>a</sup> References 10-67. Source Classification Codes in parentheses.
<sup>b</sup> Halogenated species are those containing atoms of chlorine, bromine, fluorine, or iodine. For any equipment, the control efficiency for mercury should be assumed to be 0. See section 2.4.4.2 for methods to estimate emissions of SO<sub>2</sub>, CO<sub>2</sub>, and HCl.

<sup>&</sup>lt;sup>c</sup> Where information on equipment was given in the reference, test data were taken from enclosed flares. Control efficiencies are assumed to be equally representative of open flares.

Table 2.4-4. (Metric Units) EMISSION FACTORS FOR SECONDARY COMPOUNDS EXITING CONTROL DEVICES<sup>a</sup>

Control Device	Pollutant <sup>b</sup>	Typical Rate, kg/hr/dscmm Methane	Emission Factor Rating
Flare <sup>c</sup>	Nitrogen dioxide	0.039	С
(50100410)	Carbon monoxide	0.72	C
(50300601)	Particulate matter	0.016	D
IC Engine	Nitrogen dioxide	0.24	D
(50100421)	Carbon monoxide	0.45	C
,	Particulate matter	0.046	E
Boiler/Steam Turbine <sup>d</sup>	Nitrogen dioxide	0.032	D
(50100423)	Carbon monoxide	$5.4 \times 10^{-3}$	Е
,	Particulate matter	$7.9 \times 10^{-3}$	D
Gas Turbine	Nitrogen dioxide	0.083	D
(50100420)	Carbon monoxide	0.22	Е
	Particulate matter	0.021	Е

<sup>&</sup>lt;sup>a</sup> Source Classification Codes in parentheses.

<sup>&</sup>lt;sup>b</sup> No data on PM size distributions were available, however for other gas-fired combustion sources, most of the particulate matter is less than 2.5 microns in diameter. Hence, this emission factor can be used to provide estimates of PM-10 or PM-2.5 emissions. See section 2.4.4.2 for methods to estimate CO<sub>2</sub>, SO<sub>2</sub>, and HCl.

<sup>&</sup>lt;sup>c</sup> Where information on equipment was given in the reference, test data were taken from enclosed flares. Control efficiencies are assumed to be equally representative of open flares.

 $<sup>^{\</sup>rm d}$  All source tests were conducted on boilers, however emission factors should also be representative of steam turbines. Emission factors are representative of boilers equipped with low-NO<sub>x</sub> burners and flue gas recirculation. No data were available for uncontrolled NO<sub>x</sub> emissions.

Table 2.4-5. (English Units) EMISSION RATES FOR SECONDARY COMPOUNDS EXITING CONTROL DEVICES<sup>a</sup>

Control Device	Pollutant <sup>b</sup>	Typical Rate, lb/hr/dscfm Methane	Emission Factor Rating
Flare <sup>c</sup> (50100410) (50300601)	Nitrogen dioxide Carbon monoxide Particulate matter	$2.4 \times 10^{-3} 0.045 1.0 \times 10^{-3}$	C C D
IC Engine (50100421)	Nitrogen dioxide	0.015	D
	Carbon monoxide	0.028	C
	Particulate matter	2.9 x 10 <sup>-3</sup>	E
Boiler/Steam Turbine <sup>d</sup> (50100423)	Nitrogen dioxide	2.0 x 10 <sup>-3</sup>	E
	Carbon monoxide	3.4 x 10 <sup>-4</sup>	E
	Particulate matter	4.9 x 10 <sup>-4</sup>	E
Gas Turbine (50100420)	Nitrogen dioxide	5.2 x 10 <sup>-3</sup>	D
	Carbon monoxide	0.014	D
	Particulate matter	1.3 x 10 <sup>-3</sup>	E

<sup>&</sup>lt;sup>a</sup> Source Classification Codes in parentheses.

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<sup>&</sup>lt;sup>b</sup> Based on data for other combustion sources, most of the particulate matter will be less than 2.5 microns in diameter. Hence, this emission rate can be used to provide estimates of PM-10 or PM-2.5 emissions. See section 2.4.4.2 for methods to estimate CO<sub>2</sub>, SO<sub>2</sub>, and HCl.

<sup>&</sup>lt;sup>c</sup> Where information on equipment was given in the reference, test data were taken from enclosed flares. Control efficiencies are assumed to be equally representative of open flares.

 $<sup>^{\</sup>rm d}$  All source tests were conducted on boilers, however emission factors should also be representative of steam turbines. Emission factors are representative of boilers equipped with low-NO<sub>x</sub> burners and flue gas recirculation. No data were available for uncontrolled NO<sub>x</sub> emissions.

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